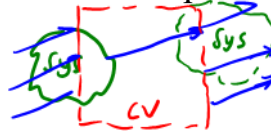


# REYNOLDS TRANSPORT THEOREM

In this lesson, we will:

- Show an analogy between the material derivative and the **Reynolds Transport Theorem**
- Discuss the purpose and usefulness of the Reynolds Transport Theorem (RTT)
- Show alternate forms of the RTT, including various simplifications
- Do an example problem

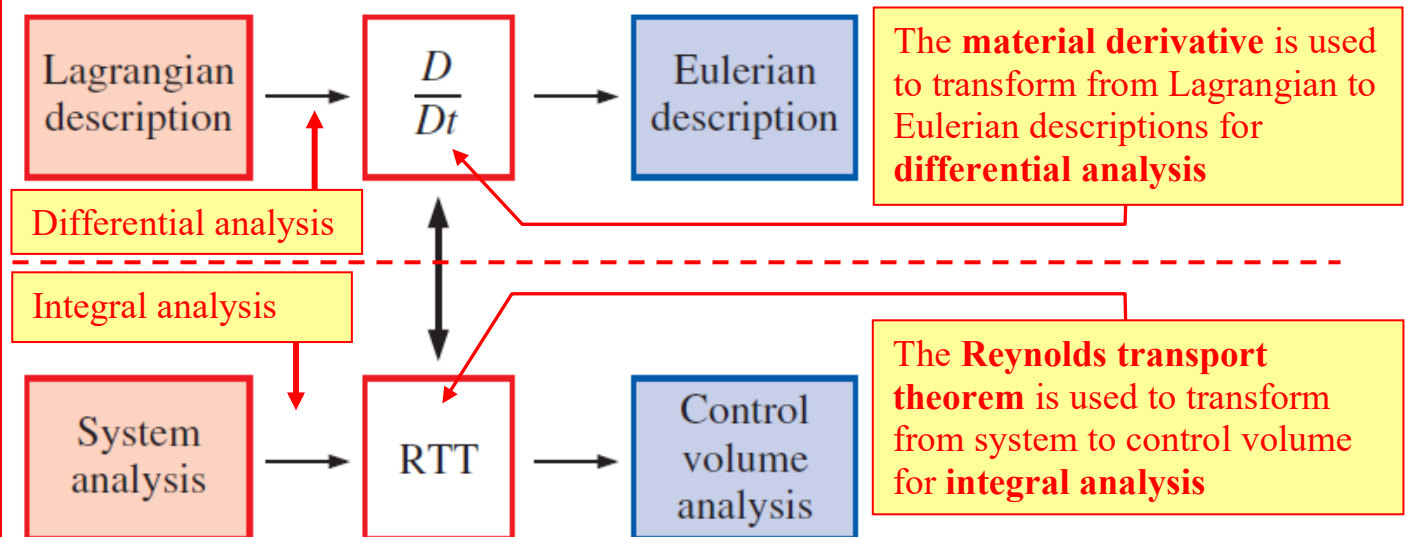


## Introduction and Overview

- A **system** [also called a **closed system**] is a quantity of matter of fixed identity. **No mass can cross a system boundary.**
- A **control volume** [also called an **open system**] is a region in space chosen for study. **Mass can cross a control surface** (the surface of the control volume).
- The fundamental conservation laws (conservation of mass, energy, etc.) *apply directly to systems.*
- However, in most fluid mechanics problems, **control volume analysis is preferred over system analysis** (for the same reason that the Eulerian description is usually preferred over the Lagrangian description).
- Therefore, we need to **transform the conservation laws from a system to a control volume.** This is accomplished with the **Reynolds transport theorem (RTT).**

## Analogy Between the Material Derivative and the RTT

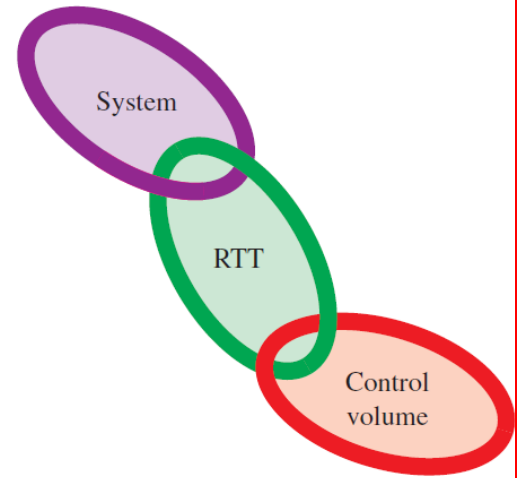
There is a direct **analogy** between the transformation from **Lagrangian** to **Eulerian** descriptions (**for differential analysis** using infinitesimally small fluid elements) and the transformation from **systems** to **control volumes** (**for integral analysis** using large, finite flow fields):



In both cases, the fundamental laws of physics (conservation laws) are **known** and apply directly to the analysis on the left (Lagrangian or system).

These laws of physics must be **transformed** so as to be useful in the analysis on the right (Eulerian or control volume).

Another way to think about the RTT is that it is a **link** between the system approach and the control volume approach.



See textbook for detailed derivation of the RTT. Here are some highlights:

*B can be a scalar or a vector*

- Let  $B$  represent any **extensive property** (like mass, energy, or momentum).
- Let  $b$  be the corresponding **intensive property**, i.e.,  $b = B/m$  (property  $B$  per unit mass).
- Our goal is to find a relationship between  $B_{\text{sys}}$  or  $b_{\text{sys}}$  (property of the system, for which we know the conservation laws) and  $B_{\text{CV}}$  or  $b_{\text{CV}}$  (property of the control volume, which we prefer to use in our analysis).
- The results are shown below in various forms:

For **fixed** (non-moving and non-deforming) control volumes,

*RTT, fixed CV:*

$$\frac{dB_{\text{sys}}}{dt} = \frac{d}{dt} \int_{\text{CV}} \rho b \, dV + \int_{\text{CS}} \rho b \vec{V} \cdot \vec{n} \, dA \quad (4-41)$$

*change of  $B_{\text{sys}}$  due to unsteadiness*

*change of  $B_{\text{sys}}$  due to movement of fluid across the C.S. (4-41)*

*unit outward normal vector*

*Alternate RTT, fixed CV:*

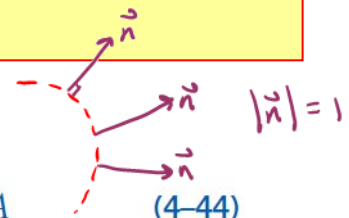
$$\frac{dB_{\text{sys}}}{dt} = \int_{\text{CV}} \frac{\partial}{\partial t} (\rho b) \, dV + \int_{\text{CS}} \rho b \vec{V} \cdot \vec{n} \, dA \quad (4-42)$$

Since the control volume is **fixed**, the order of integration or differentiation does not matter, i.e.,  $\frac{d}{dt} \int_{\text{CV}} \dots$  is the same as  $\int_{\text{CV}} \frac{\partial}{\partial t} \dots$ . Thus, the two circled quantities above are **equivalent** for a fixed control volume.

For **nonfixed** (moving and/or deforming) control volumes,

*RTT, nonfixed CV:*

$$\frac{dB_{\text{sys}}}{dt} = \frac{d}{dt} \int_{\text{CV}} \rho b \, dV + \int_{\text{CS}} \rho b \vec{V}_r \cdot \vec{n} \, dA \quad (4-44)$$

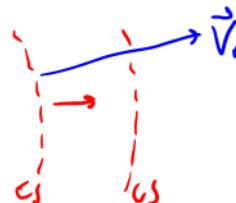


*Note: The only difference in the equations is that we replace  $\vec{V}$  by  $\vec{V}_r$  in this version of the RTT for a moving and/or deforming control volume.*

where  $\vec{V}_r$  is the **relative velocity**, i.e., the velocity of the fluid *relative to the control surface* (which may be moving or deforming),

*Relative velocity:*

$$\vec{V}_r = \vec{V} - \vec{V}_{\text{CS}} \quad (4-43)$$



We can also switch the order of the time derivative and the integral in the first term on the right, but only if we use the *absolute* (rather than the relative) velocity in the second term on the right, i.e.,

*Alternate RTT, nonfixed CV:* 
$$\frac{dB_{\text{sys}}}{dt} = \int_{\text{CV}} \frac{\partial}{\partial t} (\rho b) dV + \int_{\text{CS}} \rho b \vec{V} \cdot \vec{n} dA \quad (4-45)$$

Comparing Eqs. 4-45 and 4-42, we see that they are identical. Thus, the most general form of the RTT that *applies to both fixed and non-fixed control volumes* is

*General RTT, nonfixed CV:* 
$$\frac{dB_{\text{sys}}}{dt} = \int_{\text{CV}} \frac{\partial}{\partial t} (\rho b) dV + \int_{\text{CS}} \rho b \vec{V} \cdot \vec{n} dA \quad (4-53)$$

Even though this equation is most general, it is often easier *in practice* to use Eq. 4-44 for moving and/or deforming (non-fixed) control volumes because the algebra is easier.

### Simplifications:

- For **steady** flow, the volume integral drops out. In terms of relative velocity,

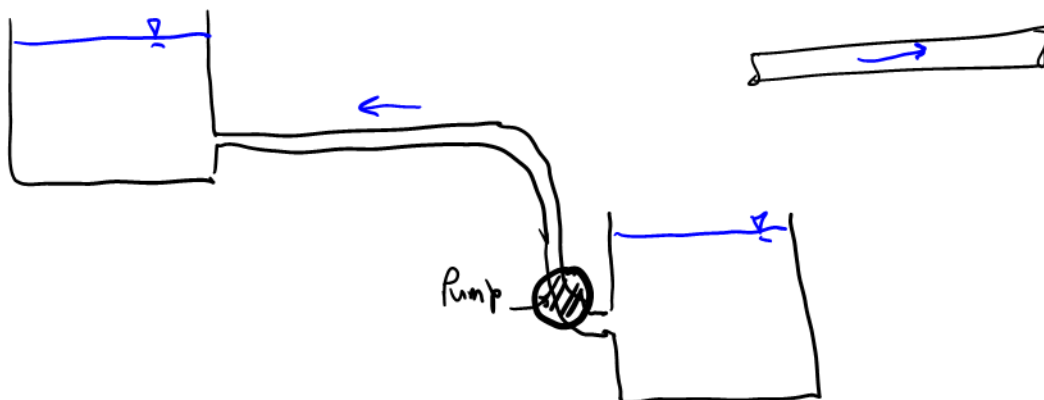
*RTT, steady flow:* 
$$\frac{dB_{\text{sys}}}{dt} = \oint_{\text{CS}} \rho b \vec{V}_r \cdot \vec{n} dA \quad (4-46)$$
 indicate integration over the entire CS

- For control volumes where there are **well-defined inlets and outlets**, the control surface integral can be simplified, avoiding cumbersome integrations,

*Approximate RTT for well-defined inlets and outlets:*

$$\frac{dB_{\text{sys}}}{dt} = \frac{d}{dt} \int_{\text{CV}} \rho b dV + \sum_{\text{out}} \underbrace{\rho_{\text{avg}} b_{\text{avg}} V_{r,\text{avg}} A}_{\text{for each outlet}} - \sum_{\text{in}} \underbrace{\rho_{\text{avg}} b_{\text{avg}} V_{r,\text{avg}} A}_{\text{for each inlet}} \quad (4-48)$$

Note that the above equation is *approximate*, so it may not always be accurate; but it will be used almost exclusively in this course and is used generally in engineering analysis.

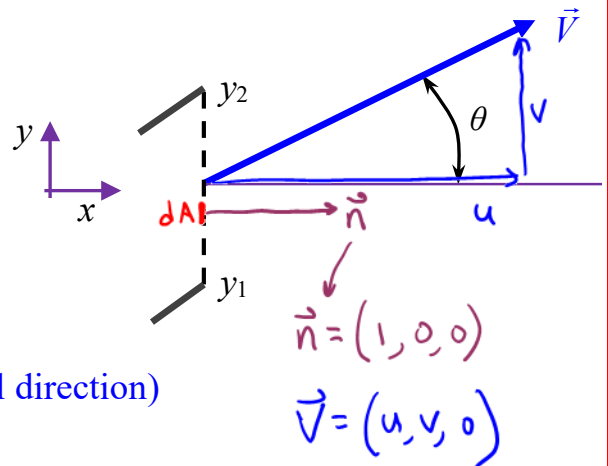


Something we need to integrate over a portion of the CS.

### Example: Reynolds Transport Theorem

**Given:** There is a steady, two-dimensional flow of water (density = 1000 kg/m<sup>3</sup>) out of a large outlet as sketched (not to scale).

- Location  $y_1 = 1.00$  m
- Location  $y_2 = 3.00$  m
- Property  $b$  in the RTT equation is  $(1)$
- The width of the outlet (into the page in the sketch) is  $s = 10.0$  m
- The velocity components are  $u = 3.22$  m/s (horizontal direction) and  $v = 1.50$  m/s (vertical direction)
- The velocity is constant across the entire outlet



**To do:** Calculate the RTT surface integral  $\int_{\text{outlet}} \rho b (\vec{V} \cdot \vec{n}) dA$  across this outlet.

**Solution:**

$$\begin{aligned} \vec{V} \cdot \vec{n} &= (u, v, 0) \cdot (1, 0, 0) \\ &= u(1) + v(0) + 0(0) \end{aligned}$$

$$\vec{V} \cdot \vec{n} = u$$

$$\int_{\text{outlet}} \rho b (\vec{V} \cdot \vec{n}) dA = \rho b u s \int_{y_1}^{y_2} dy = \rho b u s (y_2 - y_1)$$

#5:

$$\begin{aligned} \int_{\text{outlet}} \rho b (\vec{V} \cdot \vec{n}) dA &= \left( 1000 \frac{\text{kg}}{\text{m}^3} \right) (1) \left( 3.22 \frac{\text{m}}{\text{s}} \right) (10.0 \text{ m}) (3.00 - 1.00) \text{ m} \\ &= 64,400 \frac{\text{kg}}{\text{s}} \end{aligned}$$

Handwritten notes for the calculation:

- $(b = \frac{m}{m})$  ( $B = m$ )