

Chapter 4 of Heinsohn & Cimbala: Useful Tables

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Table 4.3 Convection heat transfer and mass transfer relationships (abstracted from Bird et al., 1960 and Incropera and DeWitt, 1990).

1. Air flowing over a flat surface $Nu = \frac{Lh}{k}$ $Pr = \frac{c_p \mu}{k}$ $Re = \frac{\rho U_\infty L}{\mu}$

Laminar flow: $Pr > 0.6$ $Re < 5 \times 10^5$ $Nu = 0.664(Re)^{0.5} (Pr)^{0.33}$

Turbulent flow: $0.6 < Pr < 60$ $5 \times 10^5 < Re < 10^8$ $Nu = (0.037(Re)^{0.80} - 871)(Pr)^{0.33}$

2. Air flowing through a cylindrical duct $Sh = k_G \frac{R_u TLP_{am}}{D_{ja} P}$

Turbulent flow: $0.6 < Sc < 300$ $4,000 < Re < 60,000$ $Sh = 0.023(Re)^{0.83} (Sc)^{0.33}$

3. Air flowing over a stationary sphere ($L = D$)

Laminar or turbulent flow: $0.71 < Pr < 380$ $3.5 < Re < 7.6 \times 10^4$ $1.0 < \mu_\infty/\mu_s < 3.2$

$$Nu = 2 + \left[0.4\sqrt{Re} + 0.06(Re)^{2/3} \right] (Pr)^{0.4} \left(\frac{\mu_\infty}{\mu_s} \right)^{1/4}$$

where viscosity μ_∞ is evaluated at the far-field temperature and viscosity μ_s is evaluated at the average surface temperature.

4. External flowing over plates and cylinders ($Pr > 0.7$) $Nu = C (Re)^{a_2} (Pr)^{0.33}$

	Re	C	a₂
Horizontal cylinder ($D = L$):	0.4-4	0.989	0.330
	4-40	0.911	0.385
	40-4000	0.683	0.466
	4000-40,000	0.193	0.618
	40,000-400,000	0.027	0.805
Square (L by L), flow 90° to flat surface:	5000-100,000	0.246	0.588
	Square (L by L), flow 45° to a flat surface:		
	5000-100,000	0.102	0.675
Semi-infinite vertical plate (height L) flow 90° to flat surface:			
	4000-15,000	0.288	0.731

5. Air flowing through a fixed bed of pellets $Sc = 0.6$ $\epsilon = 1 - \frac{D_p a_s}{6}$

Low Re flow: $90 < Re < 4,000$ $Nu = \frac{2.06}{\epsilon} (Re)^{0.422} Pr (Sc)^{-0.67}$

High Re flow: $5,000 < Re < 10,300$ $Nu = \frac{20.4}{\epsilon} (Re)^{0.185} (Sc)^{-0.67} Pr$

where a_s = total pellet surface area per volume of fixed bed