

Today, we will:

- Finish the example problem we started last time – converging duct
- Discuss choked flow and choking in more detail
- Discuss how to calculate the mass flow rate for converging nozzle flow

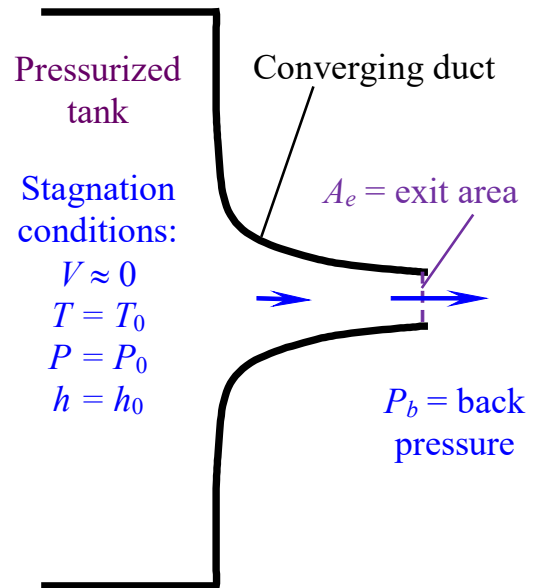
Example: Converging duct flow

Given: Air flows steadily from a large pressurized tank at pressure P_0 into a converging duct that is open to another large tank at pressure P_b . The duct is insulated and we ignore friction. We measure:

- $P_0 = 158.0$ kPa
- $T_0 = 520.0$ K
- $P_b =$ back pressure = 101.3 kPa
- $A_e =$ exit area = 0.0130 m²

To do:

- Is the flow at the exit subsonic, sonic, or supersonic?
- Calculate M_e and T_e for this case.
- As we lower back pressure, at what value of P_b does the nozzle exit become sonic?
- What happens if $P_b < P^*$?

**Solution:**

Assumptions and Approximations: steady, ideal gas, adiabatic, isentropic, 1-D approx.

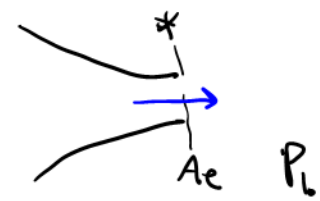
Last time we did (a) and (b):

- Flow is subsonic
- $M_e = 0.823$ (subsonic) and $T_e = 458$. K

Comments:

1. Part (b) verifies Part (a) – namely that the Mach number at the exit is subsonic.
2. The back pressure would need to be lower than the given back pressure in order to make the flow sonic at the exit plane.
3. Notice how cold the exit temperature is. We went from 520 K in the tank to 458 K at the exit plane, a drop of 62 K!
4. Critical (* or sonic) conditions do not actually occur anywhere in this flow, but critical conditions are still useful in solving problems like this.

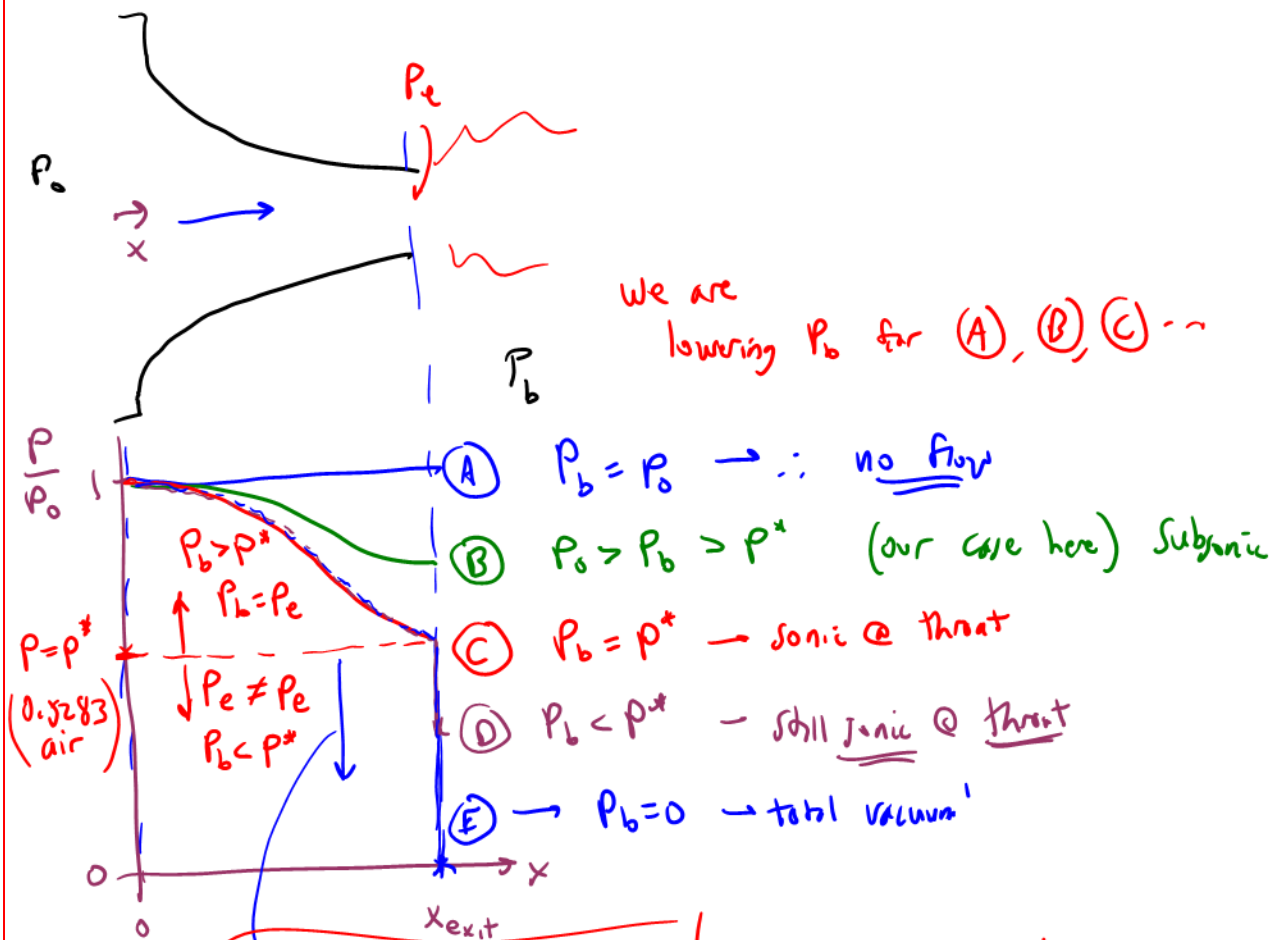
(c) Sonic when $P_b = P^* = 83.47 \text{ kPa}$



(d) IF $P_b < P^*$ what happens?

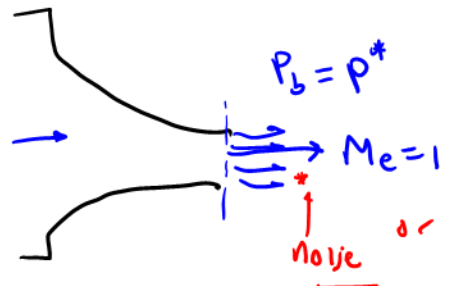
The flow stays sonic @ exit plane (throat)

Plot $\frac{P}{P_0}$ vs $P_b \downarrow$



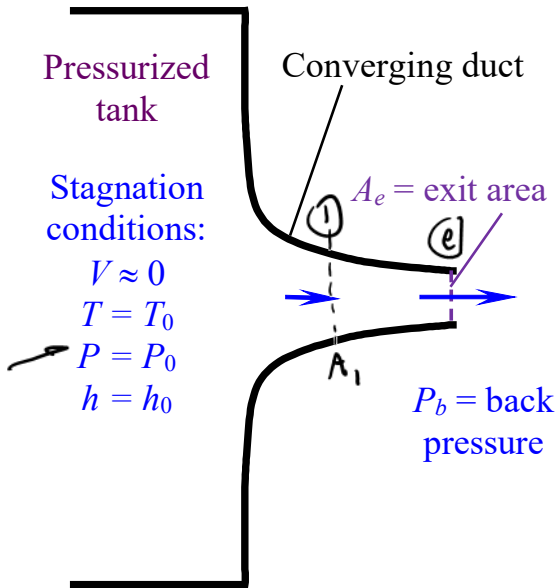
Flow is CHOKED \rightarrow if $P_b < P^*$

$M = 1$ @ exit plane
 $P_e = P^* \neq P_b$



or pressure change cannot be felt inside the nozzle

Converging nozzle (continued)



Mass flow rate \dot{m} is constant
 no matter what P_b is if
 $P_b < P^*$
Choked

Let's calculate the **mass flow rate** through the nozzle as a function of the stagnation conditions, the back pressure, and the exit area.

* General case (may or may not be choked)

Ideal gas → $\dot{m} = \rho V A$ anywhere

$$\dot{m} = \frac{P}{RT} \cdot M \cdot a \cdot A = \frac{P}{RT} M \sqrt{\gamma RT} A = \boxed{P A M \sqrt{\frac{\gamma}{RT}} = \dot{m}}$$

$a = \sqrt{\gamma RT}$

$V = Ma$

Also → Isentropic → we use isentropic relations

$$\dot{m} = P A M \sqrt{\frac{\gamma}{RT}} = \left(\frac{P}{P_0}\right) P_0 A M \sqrt{\frac{\gamma}{R}} \left[\frac{T}{T_0}\right]^{-1/2}$$

Using ratio "trick"

$$\dot{m} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{-\frac{\gamma}{\gamma-1}} P_0 A M \sqrt{\frac{\gamma}{R}} \left[\left(1 + \frac{\gamma-1}{2} M^2\right)^{-1} T_0\right]^{-1/2}$$

Combine exponents $(-)^a (-)^b = (-)^{a+b}$

$$\dot{m} = P_0 A M \sqrt{\frac{\gamma}{RT_0} \left(1 + \frac{\gamma-1}{2} M^2\right)^{-\frac{\gamma+1}{2(\gamma-1)}}} \quad (1)$$

General case
for \dot{m}
whether choked
or not

- Applies @ any cross section of the duct
- Applies even if flow is not choked
- At the exit plane, use $A = A_e$ & $M = M_e$

CHOKED CASE $\rightarrow P_b < P^* \quad A_e = A^* \quad ; \quad M = 1$

Plug in $A = A_e$, $M = 1$ into eq (1)

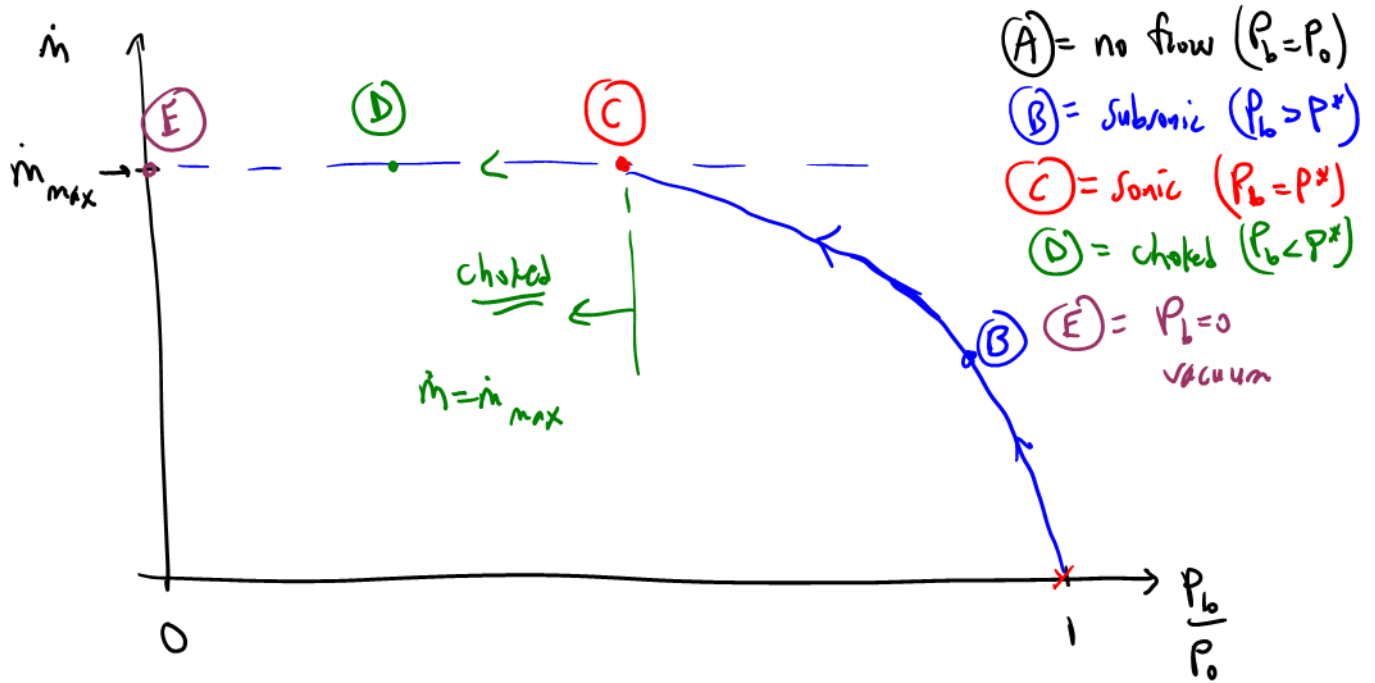
$$\dot{m}_{\text{choked}} = \dot{m}_{\text{max}} = P_0 A_e M \sqrt{\frac{\gamma}{RT_0} \left(1 + \frac{\gamma-1}{2} M^2\right)}$$

$$\dot{m}_{\text{max}} = \dot{m}_{\text{choked}} = P_0 A^* \sqrt{\frac{\gamma}{RT_0} \left(\frac{\gamma+1}{2}\right)^{-\frac{\gamma+1}{2(\gamma-1)}}}$$

\dot{m} for
choked
flow
only

Plot \dot{m} vs $\frac{P_b}{P_0}$





(Q) How to increase \dot{m} ?
 Look @ eq. for \dot{m}_{max}

$\dot{m} \uparrow$ if

- $P_0 \uparrow$ higher stag P in tank
- $A_e \uparrow$ bigger exit area
- $T_0 \downarrow$ lower T in tank (T_0)

Why $T_0 \downarrow$? $\rightarrow \rho \uparrow$ as $T_0 \downarrow$ $P_0 = \rho_0 R T_0$

But \cdot As $T_0 \downarrow$ $a = \sqrt{\gamma R T}$, $\therefore a \downarrow$
 $M = \frac{V}{a} \rightarrow$ we can achieve $M=1$
 @ a lower speed V

THIS ONE
 WINS!