

Equation Sheet for M E 521, using notation of Kundu, Cohen, and Dowling Ed. 6

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- **Tensor transformation rules for rotation:** $C_{ij} \equiv \cos \alpha_{ij}$, where α_{ij} = angle between the *old* (*i*) and *new* (*j*) axes. Then, for tensor *A*, $A'_m = C_{im} A_i$ $A'_{mn} = C_{im} C_{jn} A_{ij}$ $A'_{mnp} = C_{im} C_{jn} C_{kp} A_{ijk}$, etc.

- **Delta, epsilon, and epsilon-delta relation:** $\delta_{ij} = \vec{e}_i \cdot \vec{e}_j$ $\epsilon_{ijk} \vec{e}_k = \vec{e}_i \times \vec{e}_j$ $\epsilon_{ijk} \epsilon_{kmn} = \delta_{im} \delta_{jn} - \delta_{in} \delta_{jm}$

- **Dot product:** $\vec{a} \cdot \vec{b} = (a_i \vec{e}_i) \cdot (b_j \vec{e}_j) = a_i b_j (\vec{e}_i \cdot \vec{e}_j) = a_i b_j \delta_{ij}$ **Cross product:** $\vec{a} \times \vec{b} = \epsilon_{ijk} a_i b_j \vec{e}_k$ or $(\vec{a} \times \vec{b})_k = \epsilon_{ijk} a_i b_j$

- **Gauss (G), Stokes (S), and Leibniz (L) theorems:**

$$\text{G: } \int_V \frac{\partial F}{\partial x_i} dV = \oint_A F dA_i \quad \text{S: } \int_A (\vec{\nabla} \times \vec{u}) \cdot d\vec{A} = \oint_C \vec{u} \cdot d\vec{s} = \Gamma \quad \text{L: } \frac{d}{dt} \int_{V(t)} F(\vec{x}, t) dV = \int_{V(t)} \frac{\partial F(\vec{x}, t)}{\partial t} dV + \oint_{A(t)} F(\vec{x}, t) \vec{u}_A \cdot d\vec{A}$$

- **Material derivative:** $\frac{DF}{Dt} = \frac{\partial F}{\partial t} + u_j \frac{\partial F}{\partial x_j}$ (following a fluid particle) where *F* is some variable

- **Strain rate tensor:** $S_{ij} = \frac{1}{2}(u_{i,j} + u_{j,i})$ for any fluid. Principal strain rates (eigenvalues) found from $\det |S_{ij} - \lambda \delta_{ij}| = 0$

- **Reynolds transport theorem:** $\frac{D}{Dt} \int_{V(t)} F dV = \int_{CV} \frac{\partial F}{\partial t} dV + \oint_{CS} F u_j dA_j$ where *F* can be any quantity per unit volume

- **Conservation of mass:** $0 = \int_{CV} \frac{\partial \rho}{\partial t} dV + \oint_{CS} \rho u_j dA_j$ $\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i} (\rho u_i) = 0$

- **Linear momentum equation:**

$$\text{For any fluid: } \int_{CV} \frac{\partial}{\partial t} (\rho u_i) dV + \oint_{CS} \rho u_i u_j dA_j = \int_{CV} \rho g_i dV + \oint_{CS} T_{ij} dA_j$$

$$\text{Differential form: } \frac{\partial}{\partial t} (\rho u_i) + \frac{\partial}{\partial x_j} (\rho u_i u_j) = \rho g_i + \frac{\partial T_{ij}}{\partial x_j} \quad \text{or} \quad \rho \frac{Du_i}{Dt} = \rho g_i + \frac{\partial T_{ij}}{\partial x_j} \quad (\text{this equation is called Cauchy's equation})$$

Constitutive equation (relation between stress and strain), with τ_{ij} defined as the *deviatoric stress tensor*: $T_{ij} = -p \delta_{ij} + \tau_{ij}$

For *Newtonian* fluid: $T_{ij} = -p \delta_{ij} + 2\mu S_{ij} + \lambda S_{mm} \delta_{ij}$, and the famous **Navier-Stokes equation** results:

$$\text{For compressible flow: } \rho \left(\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} \right) = -\frac{\partial p}{\partial x_i} + \rho g_i + \frac{\partial}{\partial x_j} \left[\mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right] + \frac{\partial}{\partial x_i} \left(\lambda \frac{\partial u_j}{\partial x_j} \right)$$

$$\text{For incompressible flow: } \tau_{ij} = 2\mu S_{ij} \quad T_{ij} = -p \delta_{ij} + 2\mu S_{ij} \quad \rho \left(\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} \right) = -\frac{\partial p}{\partial x_i} + \rho g_i + \mu \frac{\partial^2 u_i}{\partial x_j \partial x_j}$$

- **Useful equations for incompressible flow in Cartesian coordinates (*x, y, z*), (*u, v, w*):**

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad \nabla^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} \quad \vec{u} \cdot \vec{\nabla} = u \frac{\partial}{\partial x} + v \frac{\partial}{\partial y} + w \frac{\partial}{\partial z}$$

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = -\frac{\partial p}{\partial x} + \rho g_x + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$\rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = -\frac{\partial p}{\partial y} + \rho g_y + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right)$$

$$\rho \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{\partial p}{\partial z} + \rho g_z + \mu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$$

$$S_{xx} = \frac{\partial u}{\partial x} = \frac{1}{2\mu} \tau_{xx} \quad S_{xy} = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) = \frac{1}{2\mu} \tau_{xy} \quad S_{yy} = \frac{\partial v}{\partial y} = \frac{1}{2\mu} \tau_{yy}$$

$$\text{Vorticity: } \vec{\omega} = \vec{\nabla} \times \vec{u} \quad \text{or} \quad \omega_k = \epsilon_{ijk} \frac{\partial u_j}{\partial x_i} \quad \text{with components} \quad \omega_x = \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \quad \omega_y = \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} \quad \omega_z = \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}$$

- Useful equations for incompressible flow in cylindrical coordinates (r, θ, z) , (u_r, u_θ, u_z) :

$$\frac{1}{r} \frac{\partial}{\partial r}(ru_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(u_\theta) + \frac{\partial}{\partial z}(u_z) = 0 \quad \nabla^2 = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} + \frac{\partial^2}{\partial z^2} \quad \vec{u} \cdot \vec{\nabla} = u_r \frac{\partial}{\partial r} + \frac{u_\theta}{r} \frac{\partial}{\partial \theta} + u_z \frac{\partial}{\partial z}$$

$$\frac{\partial u_r}{\partial t} + u_r \frac{\partial u_r}{\partial r} + \frac{u_\theta}{r} \frac{\partial u_r}{\partial \theta} + u_z \frac{\partial u_r}{\partial z} - \frac{u_\theta^2}{r} = -\frac{1}{\rho} \frac{\partial p}{\partial r} + g_r + \nu \left(\nabla^2 u_r - \frac{u_r}{r^2} - \frac{2}{r^2} \frac{\partial u_\theta}{\partial \theta} \right)$$

$$\frac{\partial u_\theta}{\partial t} + u_r \frac{\partial u_\theta}{\partial r} + \frac{u_\theta}{r} \frac{\partial u_\theta}{\partial \theta} + u_z \frac{\partial u_\theta}{\partial z} + \frac{u_r u_\theta}{r} = -\frac{1}{\rho r} \frac{\partial p}{\partial \theta} + g_\theta + \nu \left(\nabla^2 u_\theta - \frac{u_\theta}{r^2} + \frac{2}{r^2} \frac{\partial u_r}{\partial \theta} \right)$$

$$\frac{\partial u_z}{\partial t} + u_r \frac{\partial u_z}{\partial r} + \frac{u_\theta}{r} \frac{\partial u_z}{\partial \theta} + u_z \frac{\partial u_z}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial z} + g_z + \nu (\nabla^2 u_z)$$

$$S_{rr} = \frac{\partial u_r}{\partial r} = \frac{1}{2\mu} \tau_{rr} \quad S_{\theta\theta} = \frac{1}{r} \frac{\partial u_\theta}{\partial \theta} + \frac{u_r}{r} = \frac{1}{2\mu} \tau_{\theta\theta} \quad S_{r\theta} = \frac{r}{2} \frac{\partial}{\partial r} \left(\frac{u_\theta}{r} \right) + \frac{1}{2r} \frac{\partial u_r}{\partial \theta} = \frac{1}{2\mu} \tau_{r\theta}$$

Vorticity: $\vec{\omega} = \vec{\nabla} \times \vec{u}$, with components $\omega_r = \frac{1}{r} \frac{\partial u_z}{\partial \theta} - \frac{\partial u_\theta}{\partial z}$ $\omega_\theta = \frac{\partial u_r}{\partial z} - \frac{\partial u_z}{\partial r}$ $\omega_z = \frac{1}{r} \frac{\partial}{\partial r}(ru_\theta) - \frac{1}{r} \frac{\partial u_r}{\partial \theta}$

- Mechanical energy equation: $\frac{\partial}{\partial t} \int_{CV} (\frac{1}{2} \rho u_i u_i) dV + \oint_{CS} (\frac{1}{2} \rho u_i u_j) dA_j = \int_{CV} \rho g_i u_i dV + \oint_{CS} T_{ij} u_i dA_j + \int_{CV} p \frac{\partial u_i}{\partial x_i} dV - \int_{CV} \phi dV$

Differential form: $\frac{\partial (\frac{1}{2} \rho u_i u_i)}{\partial t} + \frac{\partial}{\partial x_j} (u_j \frac{1}{2} \rho u_i u_i) = \rho u_i g_i + \frac{\partial}{\partial x_j} (T_{ij} u_i) + p \frac{\partial u_j}{\partial x_j} - \phi$ where the rate of viscous dissipation of

kinetic energy per unit volume is $\phi \equiv \tau_{ij} \partial u_i / \partial x_j$ where deviatoric stress tensor = $\tau_{ij} = T_{ij} + p \delta_{ij}$

[Note: Kundu's textbook uses $\varepsilon \equiv \tau_{ij} S_{ij} / \rho$ as the rate of kinetic energy dissipation per unit mass.]

- First law (heat equation): Note that in the text, e (rather than the usual u) is the internal energy per unit mass.

$$\int_{CV} \frac{\partial}{\partial t} [\rho (e + \frac{1}{2} u_i u_i)] dV + \oint_{CS} \rho (e + \frac{1}{2} u_i u_i) u_j dA_j = \int_{CV} \rho g_i u_i dV + \oint_{CS} T_{ij} u_i dA_j - \oint_{CS} q_i dA_i$$

Differential form: $\rho \frac{D}{Dt} (e + \frac{1}{2} u_i u_i) = \rho u_i g_i + \frac{\partial}{\partial x_j} (T_{ij} u_i) - \frac{\partial q_i}{\partial x_i}$ $\rho \frac{De}{Dt} = -\frac{\partial q_i}{\partial x_i} - p \frac{\partial u_i}{\partial x_i} + \phi$

If incompressible: $\rho C_p \frac{DT}{Dt} = k \frac{\partial^2 T}{\partial x_i \partial x_i} + 2\mu S_{ij} S_{ij}$ If ideal gas: $\rho C_p \frac{DT}{Dt} = \frac{Dp}{Dt} + \frac{\partial}{\partial x_i} \left(k \frac{\partial T}{\partial x_i} \right) + \phi$

If ideal gas at very low Mach number: $\rho C_p \frac{DT}{Dt} \approx k \frac{\partial^2 T}{\partial x_i \partial x_i}$

Exam 1 material ends here.

- The T - ds equations of thermodynamics: $Tds = de + pdv$ $Tds = dh - vdp$ where T = temperature, p = pressure, e = specific internal energy, h = specific enthalpy, s = specific entropy, and $v = 1/\rho$ = specific volume

- Bernoulli equations: [These are the most common ones; there are many more forms not listed here.]

For incompressible, steady, irrotational flow: $\frac{p}{\rho} + \frac{1}{2} V^2 + gz = \text{constant}$ where $V^2 = u_j u_j = |\vec{u}|^2$

For incompressible, steady, inviscid flow: $\frac{p}{\rho} + \frac{1}{2} V^2 + gz = \text{constant}$ along a streamline

For steady, compressible, inviscid, irrotational, isentropic flow: $h + \frac{1}{2} V^2 + gz = \text{constant}$ where $h \equiv e + \frac{p}{\rho}$

- Boussinesq Approximation: $\rho = \rho_o [1 - \alpha (T - T_o)]$ where $\alpha = -\frac{1}{\rho} \frac{\partial \rho}{\partial T}$ = coefficient of thermal expansion and the z -

momentum equation is $\frac{Dw}{Dt} = \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = -\frac{1}{\rho_o} \frac{\partial p}{\partial z} - [1 - \alpha (T - T_o)] g + \nu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$

- **Interaction of vortices:** Velocity induced by one vortex on its neighbors: $u_\theta = \frac{\Gamma}{2\pi r}$ where $\Gamma \equiv \text{circulation} = \oint \vec{u} \cdot d\vec{s}$
- **Vorticity equation for incompressible Newtonian flow:** $\vec{\omega} = \vec{\nabla} \times \vec{u}$ $\frac{D\omega_k}{Dt} = \omega_j \frac{\partial u_k}{\partial x_j} + \nu \frac{\partial^2 \omega_k}{\partial x_j \partial x_j}$
- **Two-dimensional potential flow:** $\vec{u} = \vec{\nabla} \phi$ $u = \frac{\partial \phi}{\partial x} = \frac{\partial \psi}{\partial y}$ $v = \frac{\partial \phi}{\partial y} = -\frac{\partial \psi}{\partial x}$ $u_r = \frac{\partial \phi}{\partial r} = \frac{1}{r} \frac{\partial \psi}{\partial \theta}$ $u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = -\frac{\partial \psi}{\partial r}$
 $z \equiv x + iy = re^{i\theta}$ $z^* \equiv x - iy = re^{-i\theta}$ $i \equiv \sqrt{-1}$ $r = |z| = \sqrt{x^2 + y^2}$ $|z| = \sqrt{zz^*}$ $e^{i\theta} = \cos \theta + i \sin \theta$ $e^{-i\theta} = \cos \theta - i \sin \theta$
 Complex potential: $w(z) = \phi + i\psi$ Complex velocity: $\frac{dw}{dz} = u(x, y) - iv(x, y) = (u_r(r, \theta) - iu_\theta(r, \theta))e^{-i\theta}$ Uniform stream at angle of attack: $w = Uze^{-i\alpha}$ Line source: $w = \frac{m}{2\pi} \ln z$ Line vortex: $w = -i \frac{\Gamma}{2\pi} \ln z$ Doublet: $w = \frac{\mu}{z}$ where $\mu = \frac{m\varepsilon}{\pi}$ Power function (stagnation point, corner flows, etc.): $w = Az^n$ Lift per unit span due to a bound vortex on a closed 2-D body: $\rho U \Gamma_a$
- **Zhukhovskiy transformation:** $z = \zeta + \frac{b^2}{\zeta}$ transforms circle of radius b in ζ -plane into line of length $4b$ in z -plane
- **Axisymmetric potential flow:** $\vec{u} = \vec{\nabla} \phi$ $u_r = \frac{\partial \phi}{\partial r} = \frac{1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta}$ $u_\theta = \frac{1}{r} \frac{\partial \phi}{\partial \theta} = -\frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}$ Uniform stream: $\psi = \frac{1}{2} U r^2 \sin^2 \theta$
 Point source: $\psi = -\frac{Q}{4\pi} \cos \theta$ Doublet: $\psi = -\frac{m}{r} \sin^2 \theta$
- **Induced drag** (on a finite wing): $D_i = \int_A \frac{1}{2} \rho V^2 dA$ where $V^2 = v^2 + w^2$ in plane A somewhere far downstream of the wing
- **One-dimensional diffusion equation:** $\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2}$ vorticity diffusion from a wall goes like $\delta \sim \sqrt{\nu t}$
- **Stokes first problem** (impulsively started plate): $\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2}$ $\eta = \frac{y}{\delta(t)}$ $F(\eta) = \frac{u}{U}$ yields $\frac{\delta}{\nu} \frac{d\delta}{dt} = \frac{-F''}{\eta F'}$ with solution $\delta = \sqrt{2\nu t}$ and $F(\eta) = 1 - \text{erf}\left(\frac{\sqrt{c}}{\sqrt{2}} \eta\right)$ or $\frac{u}{U} = 1 - \text{erf}\left(\frac{y}{2\sqrt{\nu t}}\right)$ and $\omega_z = \frac{U}{\sqrt{\pi \nu t}} \exp\left(\frac{-y^2}{4\nu t}\right)$
- **Viscous decay (diffusion) of a line vortex:** $\frac{\partial u_\theta}{\partial t} = \nu \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial (ru_\theta)}{\partial r} \right]$ $u_\theta = \frac{\Gamma}{2\pi r}$ at $t = 0$ $u_\theta(r, t) = \frac{\Gamma}{2\pi r} \left[1 - e^{-\frac{r^2}{4\nu t}} \right]$

Exam 2 material ends here.

- **2-D stagnation point flow similarity solution:** $\psi = BxF(y)$ $u = BxF'(y)$ $v = -BF(y)$ $f(\eta) = F(y)\sqrt{B/\nu}$ $\eta = y\sqrt{B/\nu}$ yields $f''' + ff'' + 1 - (f')^2 = 0$
- **Stokes flow (creeping flow):** $\vec{\nabla} \cdot \vec{u} = 0$ $\vec{\nabla} p = \mu \nabla^2 \vec{u}$ (neglecting the gravity term) $\text{Drag} \sim \mu UL$ for 3-D body of length L . For a sphere, $D = 6\pi \mu Ua = 3\pi \mu UD_p$
- **2-D (r, θ) incompressible vorticity equation in z -direction:** $\frac{\partial \omega_z}{\partial t} + u_r \frac{\partial \omega_z}{\partial r} + \frac{u_\theta}{r} \frac{\partial \omega_z}{\partial \theta} = \nu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial \omega_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \omega_z}{\partial \theta^2} \right]$
- **Two-D incompressible laminar boundary layers:** $\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$ $\frac{\partial p}{\partial y} \approx 0$ $\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\partial U}{\partial t} + U \frac{\partial U}{\partial x} + \nu \frac{\partial^2 u}{\partial y^2}$

- Blasius flat plate boundary layer ($U = \text{constant}$, $dp/dx = 0$): $u = Uf'(\eta)$ $\eta = y\sqrt{\frac{U}{\nu x}}$ $f''' + cff'' = 0$, where we pick $c = 1/2$.

$$v = \frac{1}{2}\sqrt{\frac{\nu U}{x}}(\eta f' - f) = 0.860\sqrt{\frac{\nu U}{x}} \text{ as } \eta \rightarrow \infty \quad \frac{\delta_{0.99}}{x} = \frac{4.91}{\sqrt{\text{Re}_x}} \quad \frac{\delta^*}{x} = \frac{\int_0^\infty \left(1 - \frac{u}{U}\right) dy}{x} = \frac{1.72}{\sqrt{\text{Re}_x}} \quad \frac{\theta}{x} = \frac{\int_0^\infty \frac{u}{U} \left(1 - \frac{u}{U}\right) dy}{x} = \frac{0.664}{\sqrt{\text{Re}_x}}$$

where $\text{Re}_x = \frac{\rho U x}{\mu} = \frac{U x}{\nu}$. Local skin friction coefficient at some x location: $C_f = \frac{\tau_w}{\frac{1}{2}\rho U^2} = \frac{0.664}{\sqrt{\text{Re}_x}}$. Drag coefficient per unit

depth of the plate on one side of the plate only at some x location: $C_D = \frac{D}{\frac{1}{2}\rho U^2 x} = \frac{1.33}{\sqrt{\text{Re}_x}}$.

- Falkner-Skan wedge flow boundary layer similarity solution: $U(x) = Bx^m$ $u = Uf'(\eta)$ $\eta = \frac{y}{\delta_c(x)}$ yields

$$f''' + ff'' + \beta[1 - (f')^2] = 0 \text{ where } \beta \equiv \frac{\delta_c^2}{\nu} \frac{dU}{dx} \text{ and } b = \frac{1-m}{2}, C = \sqrt{\frac{\nu(2-\beta)}{B}}, \beta = \frac{2m}{1+m} \text{ or } m = \frac{\beta}{2-\beta}$$